

BtL and PtL, differences and similarities at technical level

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KIT - The Research University in the Helmholtz Association

www.kit.edu

KIT Figures and Facts



| 59 Spinoffs and Startups 371 Trainess | Campuses – 200 ha area | 368 Professors and executive scientists |
|--|-------------------------|---|
| | 24,381 Students | |
| 300 Buildings with a usable area of 478,000 m ² | | KIT budget 2019 |
| | 3,100 Doctoral students | EUR 951 million |
| 40 Patent applications | | 39% 28% State |
| | 9,398 Employees | Third- party funds |
| 1,178 international scientists | | Status: July 2020 |

Biomass to Liquid (bioliq®)







EnergyLab 2.0



Types of renewable fuels



1st generation biofuels

- Biodiesel by transesterification of vegetable oils
- Ethanol from fermentation of sugar and starch
- Biodiesel by hydroprocessing of vegetable oils
- 2nd generation biofuels
- Synthetic fuels produced from synthesis gas (Fischer Tropsch Fuels, DME, etc.)
- Ethanol from lignocellulosic biomasses via fermentation
- Pyrolysis oil upgrading by hydroprocessing
- 3rd generation (bio) fuels
- Algae, hydrogen..., Power to Liquids

TRL 9, but food versus fuel debate

TRL 5-7, direct and indirect land use change

TRL 1-5, No more limitations !

Biomass to Liquids (FT- Route)





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Fischer Tropsch Synthesis



$CO + 2H_2 \implies -(CH_2) - + H_2O$

| Parameter | Low-temperature | High-temperature | | |
|---------------------------------------|------------------------------|-------------------------|--|--|
| | FT | FT | | |
| Products | Waxes and/or diesel fuels | Gasoline, light olefins | | |
| Temperature [°C] | 220 - 250 | 330 - 350 | | |
| Pressure [bar] | 25 - 60 | 25 | | |
| CO + H ₂ conversion [%] | 60 - 93 | 85 | | |

Catalytical Reactors in FT-Synthesis





Methanol synthesis



$$CO + 2H_2 \leftrightarrow CH_3OH$$
$$CO_2 + 3H_2 \leftrightarrow CH_3OH + H_2O$$
$$CO + H_2O \leftrightarrow CO_2 + H_2$$

$$SN = \frac{(H_2 - CO_2)}{(CO + CO_2)} = 2 \text{ to } 2,1$$

Today low pressure prefered:

- **50 100 bar**
- **2**30 270 °C
- Cu/ZnO/Al₂O₃ or Cu/ZnO/Cr₂O₃

Inerts like N_2 , Ar, CH_4 as low as possible

Reactors for Methanol synthesis





http://www.linde-

engineering.com/de/process_plants/hydrogen_and_synthes is_gas_plants/gas_generation/isothermal_reactor/index.html

Wurzel, T., 2006, Lurgi MegaMethanol Technology, DGMK Conference "Synthesis Gas Chemistry", October, 4. – 6., 2006.

Reactors for Syngas Production from Biomass



Comparison PTL BTL – GTL - crude oil



| | Plant capacity | | | | |
|--------------------------------------|----------------|------------------|------------------|-------------------------|-------------------------|
| | feedstock | | product | Invest | efficiency ² |
| | kt a⁻¹ | GW ¹⁾ | GW ¹⁾ | Mio €/GW _{Pr.} | % |
| Power to Liquids ⁶⁾ (PtL) | - | 0.1 | 0.04 | ~5000 | 40 |
| Biomasse – FTS ³⁾ (BTL) | 1000 | 0.65 | 0.3 | 1500-3000 | 45 |
| Natural gas – FTS (GTL) | 3100 | 5.5 | 3.3 | 400-750 ⁴⁾ | 60 |
| Crude oil-refinery (Referenz) | 15000 | 21.8 | 19.6 | 350-500 ⁵⁾ | 90 |

 $^{\rm 1)}$ as upper heating value $\rm H_{S}$

 $^{\rm 2)}$ Definition over $\rm H_{S}$ in product and feedstock

³⁾ [Deutsche Energie-Agentur GmbH (Dena), Biomass to Liquid – BtL.

Realisation study (Summary), final report, 2006]

⁴⁾ Equivalent 25000 – 50000 US \$ b⁻¹

⁵⁾ Using German standards

⁶⁾ Typical demoprojects discussed in Germany

Conclusion



- There are many similarities between PtL and BtL, the synthesis step is almost the same, main difference are:
 - Gas composition
 - Operation mode, as BtL is steady state and PtL is fluctuating
- All reactors from BtL can be also used in PtL, some has advantages for flexible operation, like slurry reactors
- Advanced control concepts, like model based control are very interesting
- Economy of scale is one major hurdle for BtL and PtL compared to fossil technologies
- Hybrid systems, where BtL and PtL are combined could offer some advantages for locations in Europe, like winddiesel (www.winddiesel.at)

Questions ?



H₂:CO = Fischer Tropsch CO₂ - separation 2:1 Gas Condenser Dry comp. synthesis cleaning H₂: 15% Dry comp.: CO: 37% H₂: 63% High Efficiency CO: 41% CO: 31% Gas cleaning CH₄: 5% CO₂: 0% CH4: 4% H₂O: 16% °O₂ output Syngas generation Steam steam generation FT - product M separation Condenser Biomass Additional necessary Winddiesel Steam = 0,5% Equipment: CO2=99,5% These + Renewable H₂ FT unit 70% CO>-rec. = 100% generation larger steam CO₂-output = 0%

Winddiesel full load operation-Full electrolysis power

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